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# Assessment of Fire Hazard Potential within a Hot Cell

Presented by

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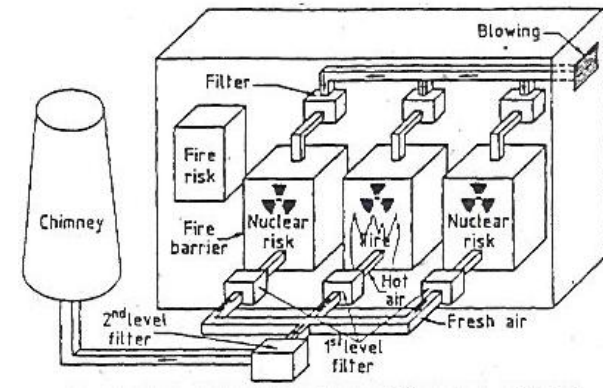
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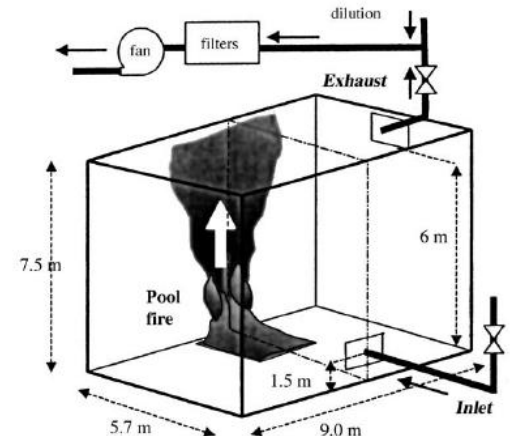
# 1. Introduction

- Forced ventilated enclosures are common in the nuclear industry.
- Recognizing the safety implications of fire within such enclosures, it is essential that accidental fires are wholly precluded by careful design and operation.

- The present study is aimed at investigating fire safety within in a typical hot cell containing a sodium cleaning system.
- Irradiated fuel subassemblies are cleaned using ethyl alcohol.
- Accidental spill of ethyl alcohol could possibly lead to an enclosure fire scenario.



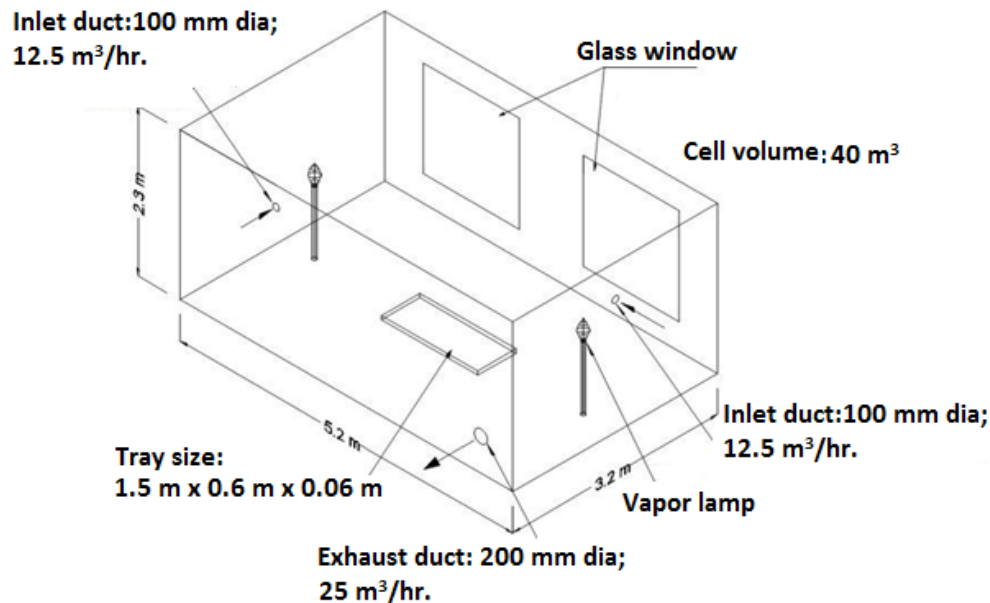
**Hot cell/glove boxes**



**Reprocessing facility**

## 2. Postulated Fire Scenario

- A scenario is envisaged wherein about 25 L of 99.9% pure ethyl alcohol spills on the leak collection tray ( $t = 0$  s).
- The initial condition within the cell: 95%  $N_2$  and 5%  $O_2$  (inert atmosphere).
- The nitrogen purging system goes out of service at time ' $t$ ' = 0 s.
- Ambient air leaks into the cell at a specified rate.
- Sodium vapor lamps are 'ON', acting as possible ignition source.

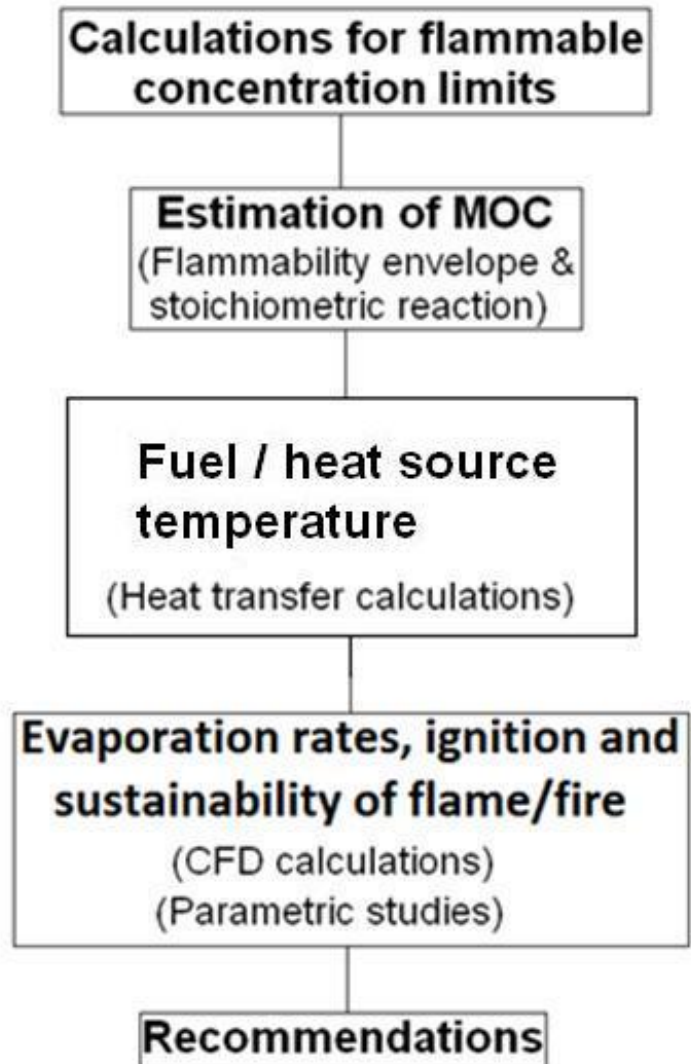


**A schematic of the hot cell**

### Objective

Assess the fire hazard potential due to inadvertent leakage, evaporation and possible ignition of ethyl alcohol vapor in the absence of nitrogen inerting.

### 3. Calculation Methodology and Tools Used



- The present investigations are carried out using appropriate mathematical models developed in-house at SRI.
- Both lumped parameter as well as CFD calculation techniques are applied.

## (a) Flammability Limits

For ethyl alcohol (flash point temperature of 13°C)

**LFL ~ 3.3 %; UFL ~ 19.2 % (% vol.)**

Quantity of vapor required to form flammable mixture within the hot cell (~ 40 m<sup>3</sup>) is calculated as follows:

$$V_e = \left[ \left( \frac{V_{cell}}{22.4 \times 10^{-3}} \right) \times \left( \frac{T_\infty}{T} \right) \times \left( \frac{P}{P_\infty} \right) \right] \times \left( \frac{LFL \text{ or } UFL}{100} \right) \times \left( \frac{MW_e}{\rho_e} \right)$$

Minimum and maximum quantity of ethanol needed to attain LFL and UFL conditions: ~ **3.09 L** and ~ **17.81 L** respectively.

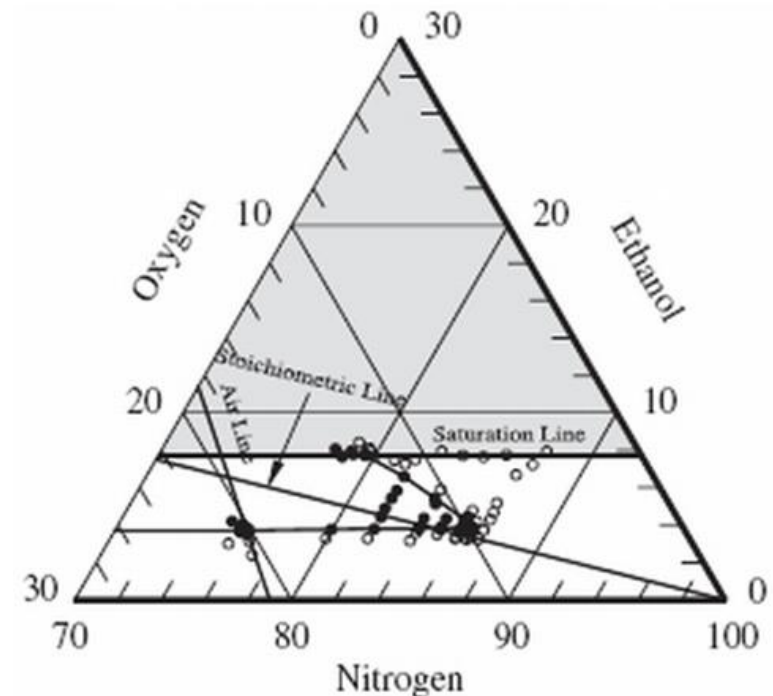
Therefore, if 25 L of ethanol completely vaporizes and mixes uniformly within the boxed-up cell, then conditions will be outside flammability limits (~ 27 % by volume).

## (b) Estimation of Minimum Oxygen Concentration (MOC)

“MOC is the limiting oxygen concentration below which premixed burning can be prevented”

- It is the oxygen concentration corresponding to the stoichiometric reaction of the lean limit fuel i.e., LFL.
- Can also be obtained from the flammability diagram.

- It is evident from the flammability diagram that MOC for ethanol vapor is around 9.9%.
- It is the lowest oxygen concentration in the entire flammability zone .



**Flammability envelop for ethanol  
at 25°C and 1 Atm.**

## (c) Lumped Parameter Model

The conservation equations for various constituent species i.e., fuel vapor, oxygen and nitrogen within the hot cell can be written as follows:

$$\frac{dY_F}{dt} = \frac{\dot{Q}_{in} \times \xi}{V_{cell}} (Y_{F,in} - Y_F) + \frac{\dot{Q}_F}{V_{cell}}$$

$$\frac{dY_{O_2}}{dt} = \frac{\dot{Q}_{in} \times \xi}{V_{cell}} (Y_{O_2,in} - Y_{O_2})$$

### Analytical solution

$$Y_F = \left[ Y_{F,in} + \frac{\dot{Q}_F}{\dot{Q}_{in} \times \xi} \right] \times \left( 1 - e^{-\left(\frac{\dot{Q}_{in} \times \xi}{V_{cell}}\right)t} \right) + Y_{F,o} \times e^{-\left(\frac{\dot{Q}_{in} \times \xi}{V_{cell}}\right)t}$$

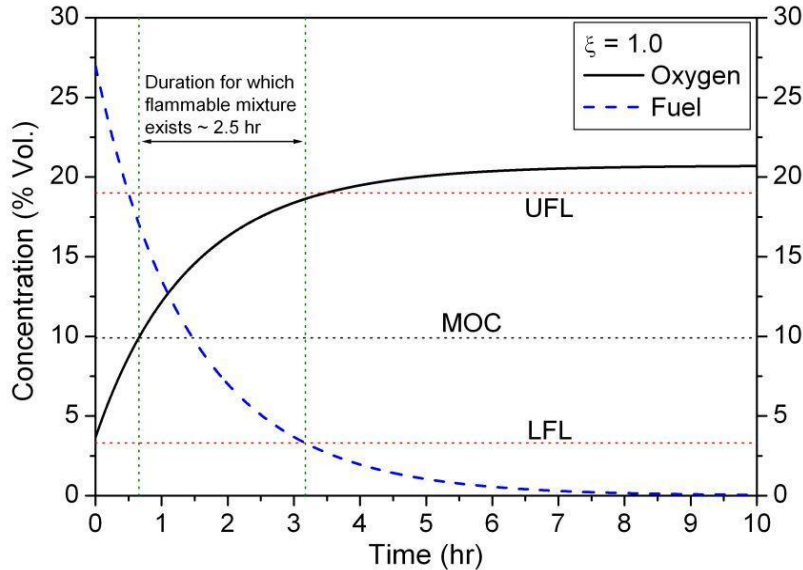
$$Y_{O_2} = Y_{O_2,in} \times \left( 1 - e^{-\left(\frac{\dot{Q}_{in} \times \xi}{V_{cell}}\right)t} \right) + Y_{O_2,o} \times e^{-\left(\frac{\dot{Q}_{in} \times \xi}{V_{cell}}\right)t}$$

$$Y_{N_2} = 1.0 - (Y_{O_2} + Y_F)$$

The variation of average mass fraction of all species can thus be obtained as a function of time.



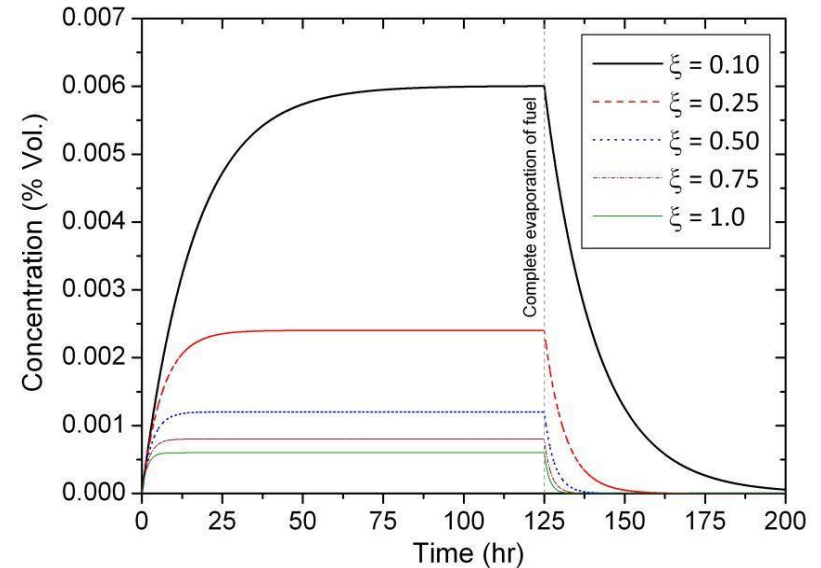
# Lumped Parameter Model



**Instantaneous mixing**

## Complete evaporation, instantaneous mixing

In this case, the spilled fuel is assumed to completely evaporate and mix with the inert cell atmosphere at time  $t=0$  s.



**Gradual mixing**

## Gradual evaporation and mixing

It is assumed that ethanol begins to evaporate at time  $t=0$  s. Therefore, no vapor is present in the cell initially.

The composition of ambient air entering the cell is taken as 79%  $N_2$  and 21%  $O_2$  in both cases.

## (d) CFD Simulations (Evaporation rate)

- The evaporation rate is estimated using an in-house CFD model.
- The average evaporation rate is calculated as follows:

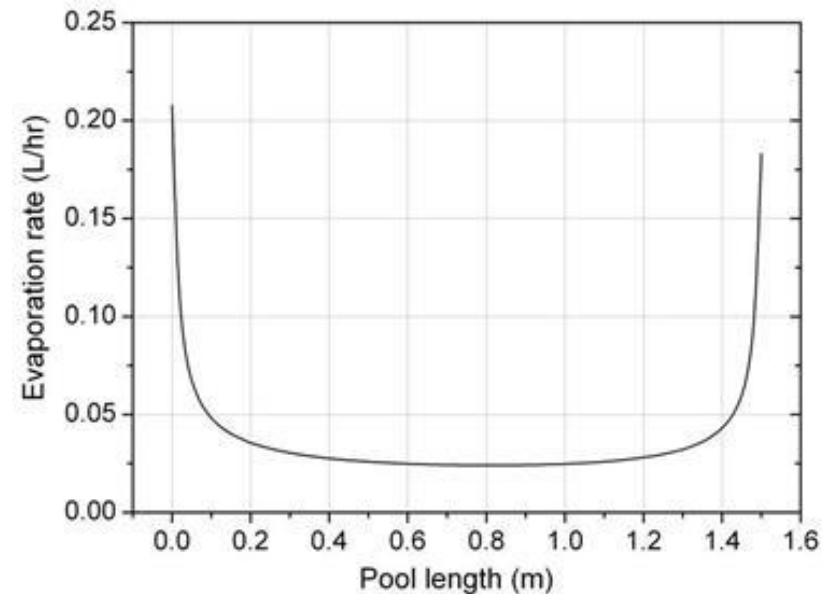
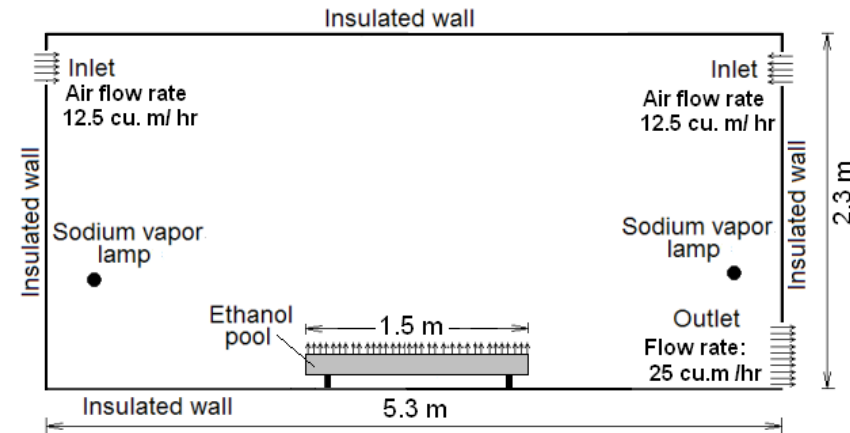
$$\overline{\dot{m}}_F'' = \frac{1}{L} \int_0^L \dot{m}_x'' dx \quad \text{kg/m}^2\text{-s}$$

On volumetric basis we can write

$$\dot{Q}_F = \frac{\overline{\dot{m}}_F'' \times L \times W}{\rho_e} \quad \text{m}^3/\text{s}$$

Average evaporation rate  $\sim 0.035$  L/hr.

For the lumped parameter calculations presented earlier, evaporation rate is conservatively taken as 0.20 L/hr.



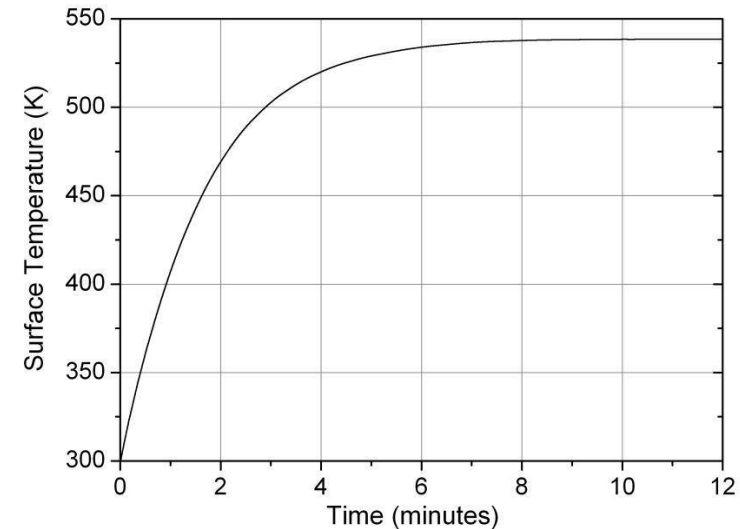
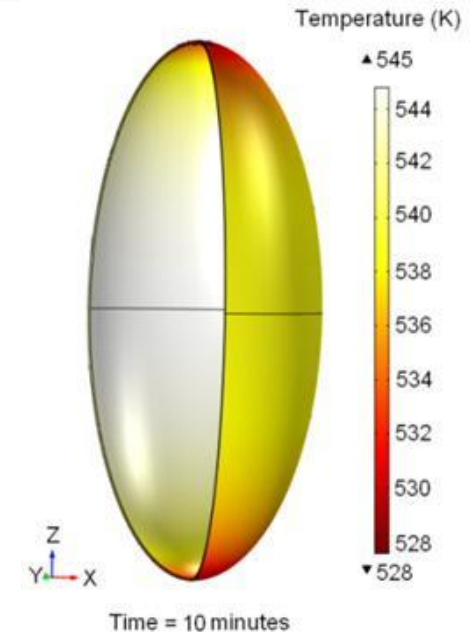
**Evaporation rate along pool length  
(Bulk liquid temperature = 30 °C)**

# CFD Simulations (Source temperature)

At this point, we seek answer to the following questions:

- How does the composition of fuel-air mixture vary near the sodium vapor lamp (heat source)?
- Will the mixture be within flammability limits, and if so, can the hot surface of lamp bulb cause ignition?

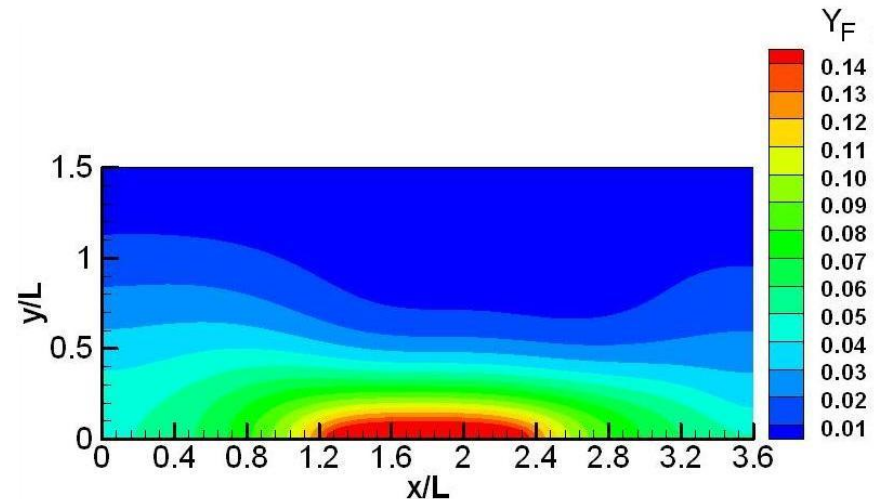
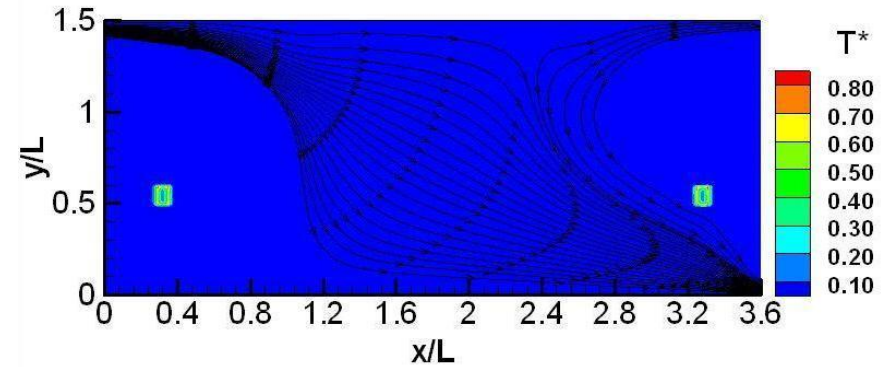
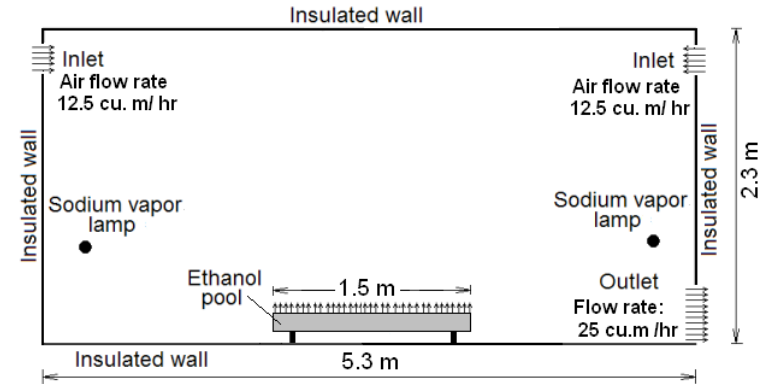
- The maximum outer surface temperature of the lamp quartz glass is estimated by solving the transient energy equation, subject to appropriate boundary conditions.



**Bulb surface temperature**

# CFD Simulations (flow field and ignition)

- The fuel vapors generated from the pool surface are transported by the forced convective flow as well as by diffusion.
- Heat source at 275°C continuously attempts to ignite the mixture.
- If the mixture reaches flammability limit near the source, ignition and subsequent burning will occur.



## 4. Summary and Recommendations

- For instantaneous mixing case, the duration for which flammable mixture exists is around 2.5 hrs.
- If partial mixing is assumed, the duration will increase.
- For the case of gradual evaporation of ethanol, the mixture remains well below the LFL. (More realistic case)
- Prevailing air flow pattern has two effects: (a) mixing, (b) cooling of source. (Both are beneficial)
- The effect of perfect mixing is to lower the average concentration of fuel vapor.
- Maintain O<sub>2</sub> concentration well within 9.9 % vol./vol., (MOC) by inerting with N<sub>2</sub>.
- Sodium vapor lamps are unlikely to act as ignition source.
- Auto ignition of ethyl alcohol vapour (365°C) is also ruled out.
- Although flammable mixture is not formed near the lamp bulb, as a safety measure put off the lamps.
- The flammability diagram of should be employed for developing a strategy to avoid fire.

Thank You